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# HEER: Liquid Salt Thermal Reactor Concept

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# Agenda

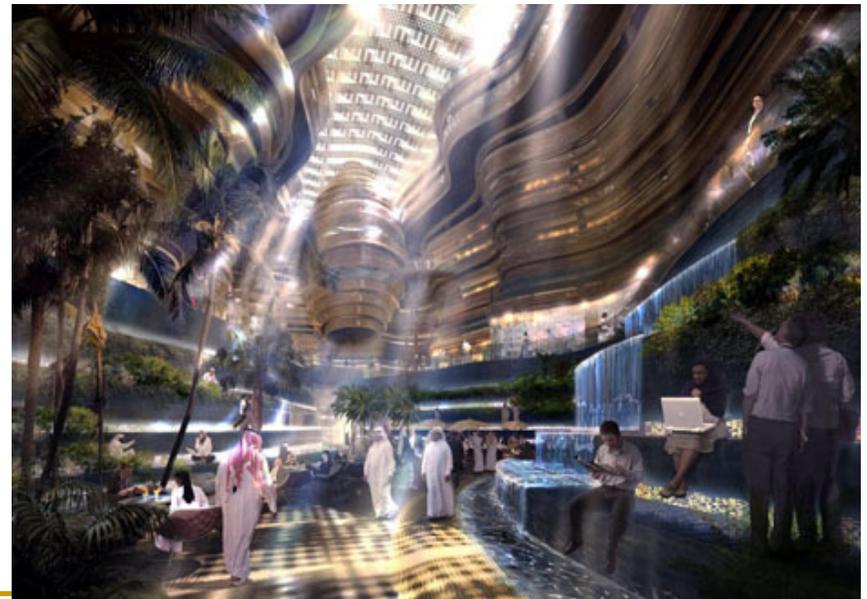
- Project Overview (2)
- Material Selection (4)
- Core Design (4)
- Performance (2)

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# Project Overview

# HEER Project Goals

- Develop a High Efficiency and Environmentally-friendly Nuclear Reactor (HEER) to address the needs of electricity, drinkable water, and hydrogen production
- Project supported by Masdar Institute of Science and Technology (Abu Dhabi, UAE) from 2007-2009
- Medium-sized reactor (1000 MWt)
- Ready for deployment worldwide → additional proliferation resistance (infrequent refueling)
- Concepts:
  - Liquid Salt Thermal Reactor
  - Annular-Fueled Superheat BWR
  - High power density IRIS



The Future MIST campus (rendered image)

# Liquid Salt Thermal Reactor

- Cool with liquid salt to avoid pressurized primary side
- Self-moderating **hydride fuel** to avoid additional moderator volume, i.e. graphite rods
- Medium enrichment (19.9 wt%) U for ~10 yr cycle length
- Supercritical CO<sub>2</sub> secondary side for high efficiency (45.7%)

Power Rating	1000 MWt (457 MWe)
Cycle Efficiency	45.7%
Peak Fuel Temperature	720°C
Coolant Outlet Temperature	570°C
Primary Coolant	Liquid Salt (NaF-BeF <sub>2</sub> )
Secondary Coolant	Supercritical CO <sub>2</sub>
Fuel Type	Hydride (U <sub>0.31</sub> ZrH <sub>1.6</sub> )
Flow Type	Integral (Dual-Free Level)

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# Material Selection

# Salt Selection Criteria

- Set up property importance criteria and weighting factors
- Point system based on rankings for each property among fluoride salts from LS-VHTR study [Ingersoll, 2006]
- Chloride salts discounted due to high thermal capture of Cl (30.5 b)

Desired property	Weighting factor
1. low melting temperature	2
2. high heat capacity	1.5
3. low viscosity	1.5
4. high thermal conductivity	1
5. low thermal capture cross section	1
6. high moderation	1
7. low volume expansion coefficient	1

# Fluoride Salt Properties at 700°C

Scoring		MP	$\rho^*C_p$	Visc.	K	n Cap.	Mod.	Vol. Exp.	total	
		[°C]	[cal/cm <sup>3</sup> °C]	[cP]	[W/mK]	Ratio <sup>1</sup>	Ratio <sup>2</sup>	Coeff.	score	
5	best	LiF-BeF <sub>2</sub>	460	1.12	5.6	1	8	60	2.52E-04	25.5
4		<b>NaF-BeF<sub>2</sub></b>	340	1.05	7	0.87	28	15	1.84E-04	23
3		LiF-NaF-BeF <sub>2</sub>	315	0.98	5	0.97	20	22	2.25E-04	32
2		LiF-ZrF <sub>4</sub>	509	0.9	>5.1	0.48	9	29	2.99E-04	9
1		NaF-ZrF <sub>4</sub>	500	0.88	5.1	0.49	24	10	2.96E-04	5
		KF-ZrF <sub>4</sub>	390	0.7	<5.1	0.45	67	3	3.17E-04	9
		RbF-ZrF <sub>4</sub>	410	0.64	5.1	0.39	14	13	3.11E-04	9.5
		LiF-NaF-ZrF <sub>4</sub>	436	0.84	6.9	0.53	20	13	3.12E-04	3
		LiF-NaF-KF	454	0.91	2.9	0.92	90	2	3.61E-04	12
		LiF-NaF-RbF	435	0.63	2.6	0.62	20	8	3.01E-04	12.5
	water (300°C)	0	0.986	0.09	0.54	75	246	3.30E-03		

<sup>1</sup> per unit volume, relative to graphite

<sup>2</sup> as calculated in [Williams et al., 2006]

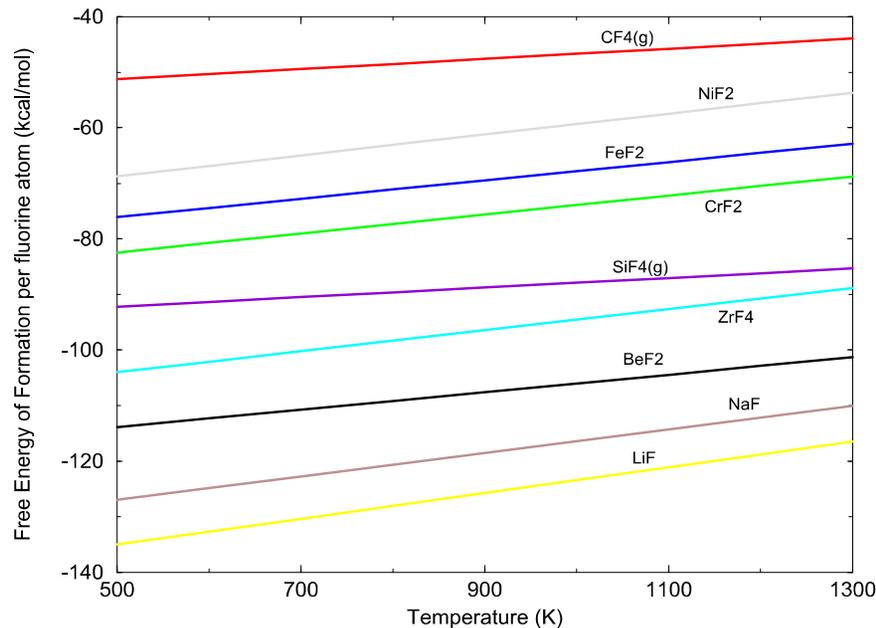
- LiF-NaF-BeF<sub>2</sub> winner but NaF-BeF<sub>2</sub> much cheaper (avoids Li<sup>7</sup> enr.)

[Williams et al., 2006]

## Material Selection (3/4)

# SiC Cladding

- Solid monolith surrounded by reinforced SiC fibers to add strength
- CVD carbon coating for salt compatibility [Sridharan, 2008]
- Strength loss saturates quickly below 1000°C (max fuel temp = 720°C)
- Thermal conductivity drops to 4 W/mK at high burnup (this was the assumed  $K$  for conservatism)



[Peterson, 2003]

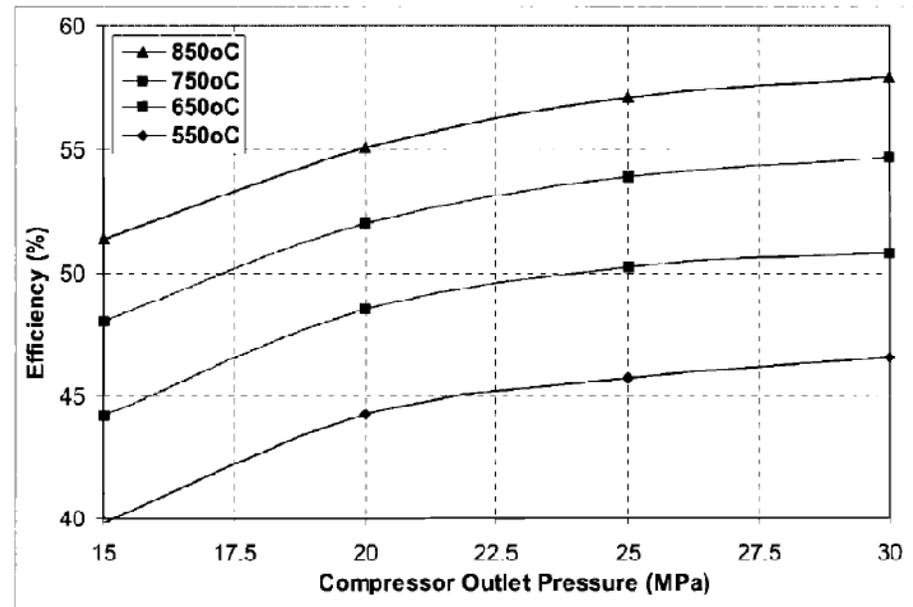
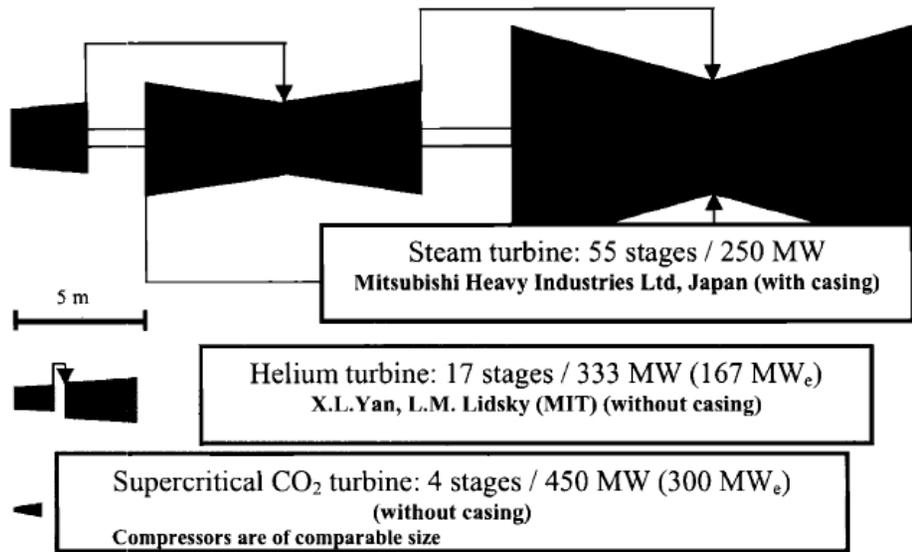


Triplex SiC cladding tube (monolith, fiber composite, and barrier coating are all SiC)

[Carpenter, 2006]

# Supercritical CO<sub>2</sub>

- Recompressive SCO<sub>2</sub> Brayton cycle
- Core outlet temperature of 570°C (set to minimize  $\Delta P$ ), 20 MPa compressor outlet pressure  $\rightarrow$  45.7% cycle efficiency
- Very compact turbine (1.5 m rotor for 300 MWe), lower capital costs



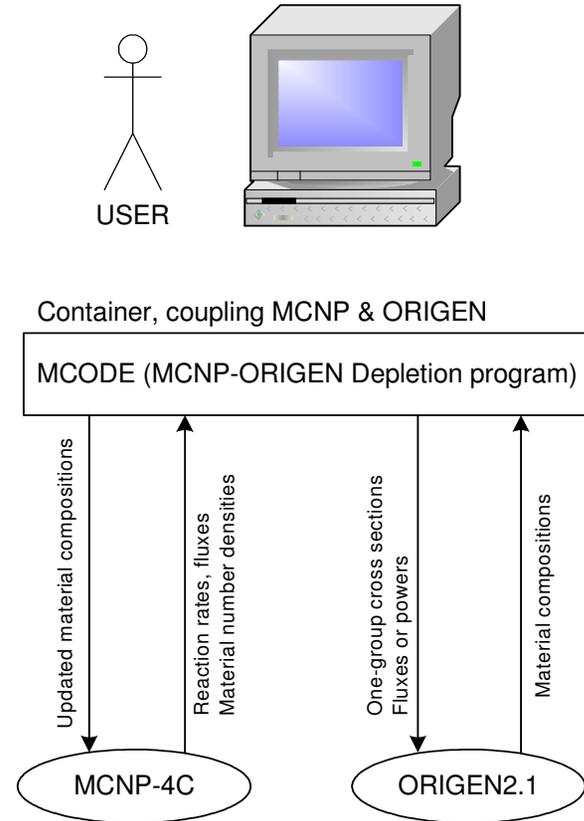
[Dostal, 2004]

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# Core Design

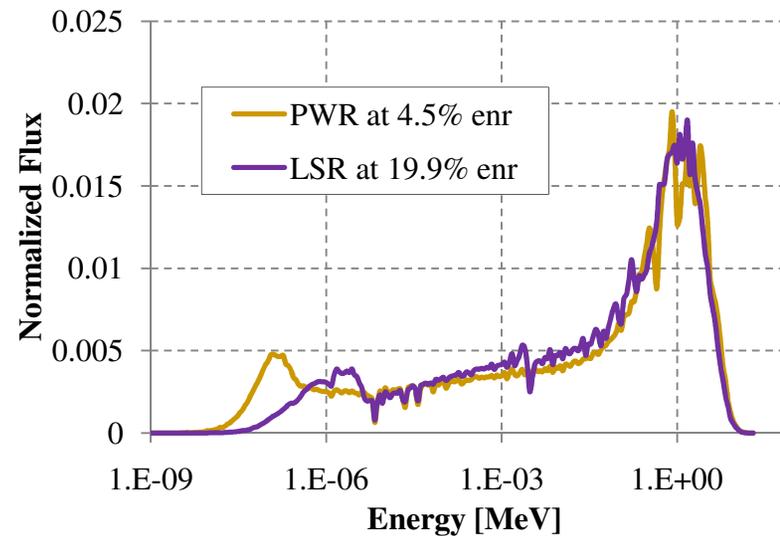
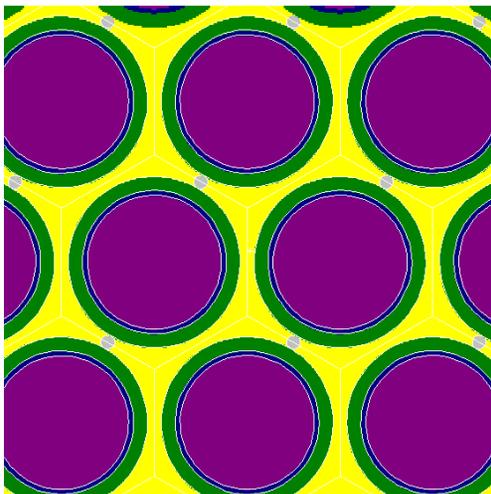
# Computational Tools

- Reactivity:  
MCNP + CASMO
- Burnup:  
MCODE (MCNP + ORIGEN)
- Thermal Hydraulics:  
iterative MATLAB scripts based on  
existing correlations



# $U_{0.31}ZrH_{1.6}$ Fuel Pins

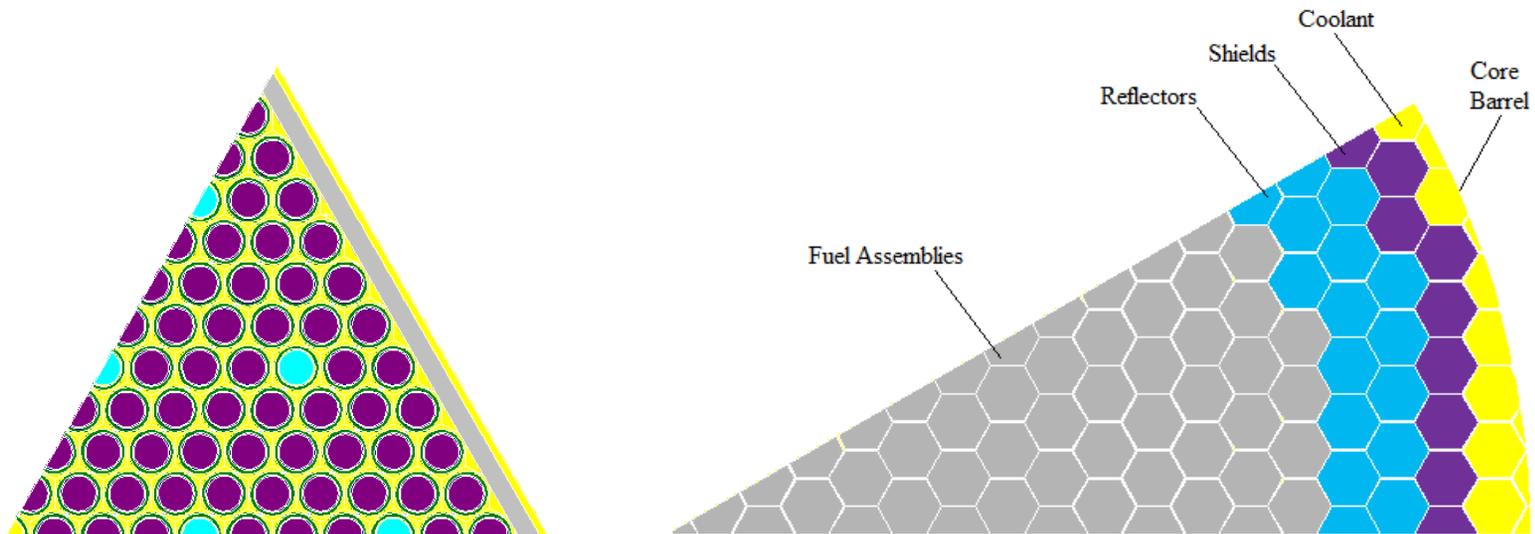
- TRIGA fuel – large prompt negative  $T_{\text{fuel}}$  feedback, high thermal conductivity (18 W/mK)
- Hydrogen diffuses out of fuel as  $T_{\text{fuel}}$  increases beyond limit
- 750°C recommended  $T_{\text{CL}}$  design limit [Simnad, 1981], set  $T_{\text{CL}} = 720^\circ\text{C}$
- Thin fuel pins (0.7 cm diam) to reduce maximum  $T_{\text{CL}}$



[Olander, 2007]  
[Simnad, 1981]

# Assembly and Core

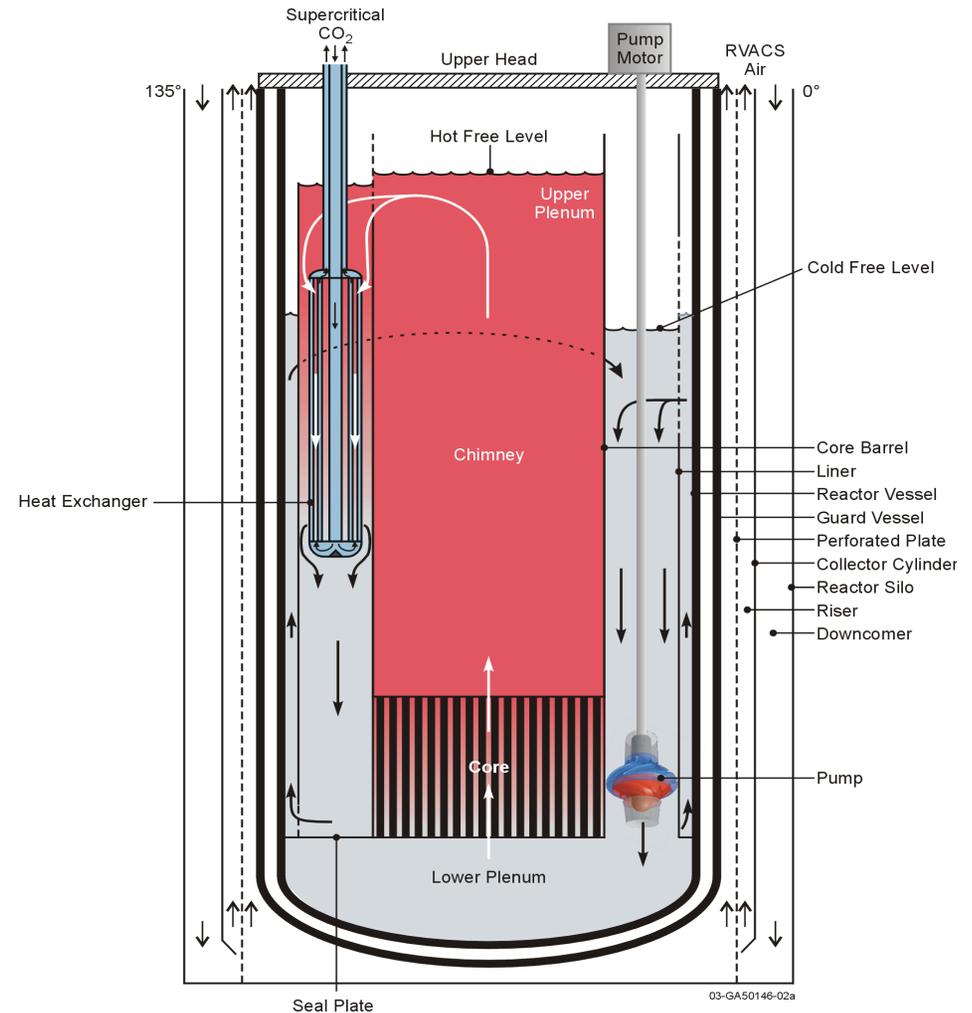
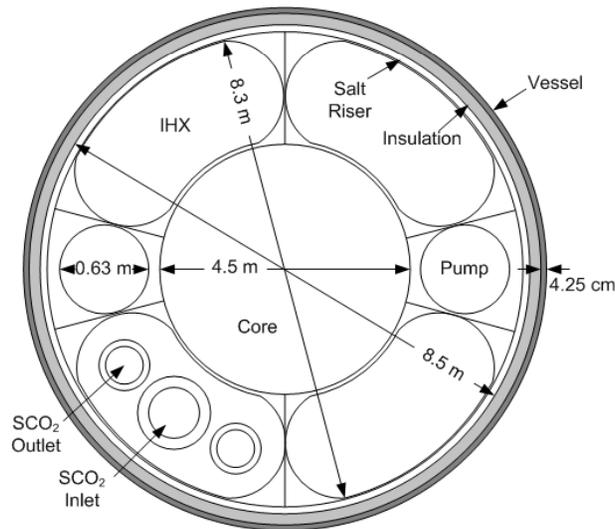
- Pins per assembly limited by assembly mass (500 kg)
- Wire wrap with Hastelloy cans to keep orificing option
- 18  $B_4C$  control rods yield roughly same worth as 24 Ag-In-Cd rods in PWR assembly (1.02 assembly ppf)
- Integral burnable poison to control excess reactivity and core radial power profile – 0.25 wt% Gd had least BU penalty (~3-4 MWd/kg)



## Core Design (4/4)

# Pool Design

- Integral design to protect against LOCAs
- Vessel diameter small enough to be built off-site and transported via rail or barge
- Dual-free level design allows CO<sub>2</sub> to escape in the event of IHX tube rupture

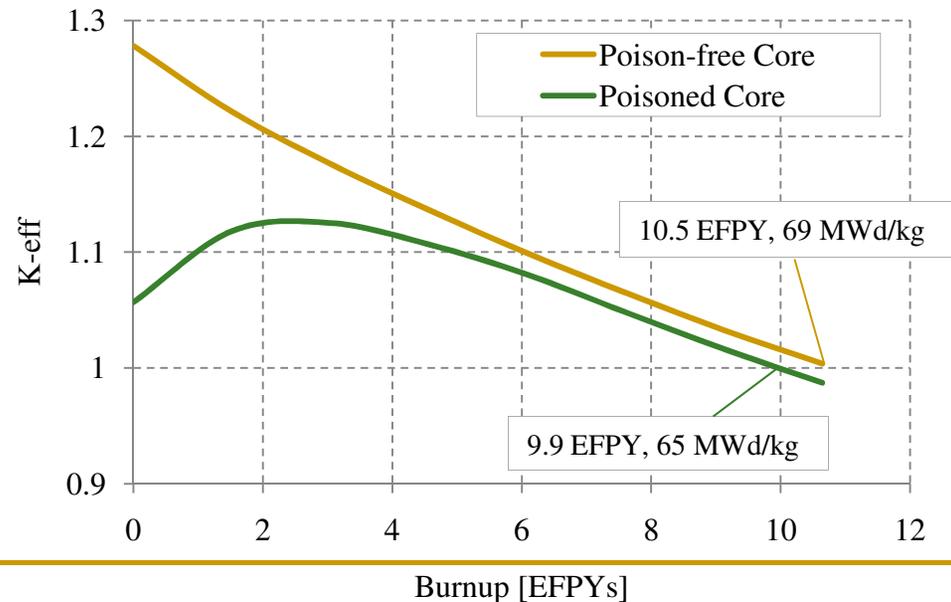


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# Performance

# Burnup Performance

- Single batch → less frequent refueling (fixed 10 EFPYs)
- Infinite pin lattice (poison-free) →  $BU_d = 98.5 \text{ MWd/kg}$ ,  $Q''' = 47 \text{ kW/L}$
- For 1000 MWt core,  $BU_d \sim 70 \text{ MWd/kg}$ ,  $Q''' = 26.4 \text{ kW/L}$  mainly due to highly-absorptive Hastelloy cans
- Using spacers (no cans) or SiC cans yields  $BU_d \sim 95 \text{ MWd/kg}$ ,  $Q''' \sim 36 \text{ kW/L}$  → smaller core diameter (8.5 m → 7.2 m)



# Conclusions

- **Proposal of a more traditional design with fluoride salt using hydride fuel rods**
- Spectrum similar to low enriched PWR (can use similar reactivity control methods)
- 10 year single batch cycle feasible with power density ~36 kW/L and ~20 wt% enrichment
- With traditional fuel pin design, Hastelloy cans are a huge neutronic penalty, should consider spacers (which precludes orificing) or inert can material (SiC)
- More data is needed on salt/cladding corrosion, multilayer cladding performance, materials for SCO<sub>2</sub>, fabrication feasibility of SiC cans, high burnup hydride fuel performance modeling
- **Bottom line: one of many options for high temperature salt application**

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# Backup Slides

# Geometry

## Pin

P/D	1.08
Pitch [cm]	0.756
Pin Diameter [cm]	0.700
Clad Thickness [cm]	0.057
Gap [cm]	0.020
Fuel Diameter [cm]	0.546
Wire Wrap Diameter [cm]	0.056

## Assembly

Rings per Asse.	11
Pins per Asse.	331
Can Thickness [cm]	0.3
Inter-Assembly Gap [cm]	0.1
Active Fuel Height [cm]	400
Inner Duct Flat-to-flat [cm]	13.85
Outer Duct Flat-to-flat [cm]	14.45
Inter-Assembly pitch [cm]	14.65
Assembly Area (incl. duct) [cm <sup>2</sup> ]	180.84

## Core

Fuel Assemblies per Core	511
Linear Power [kW/m]	1.57
Volumetric Power [kW/L]	26.35
Specific Power [kW/kgHM]	18.01
1/12 Core Fuel Volume [L]	1244.3
Power (1/12 core) [MWt]	83.44
Power (full core) [MWt]	1001.23
Discharge Burnup [MWd/kg]	69
Cycle Length [EFPY]	10.49

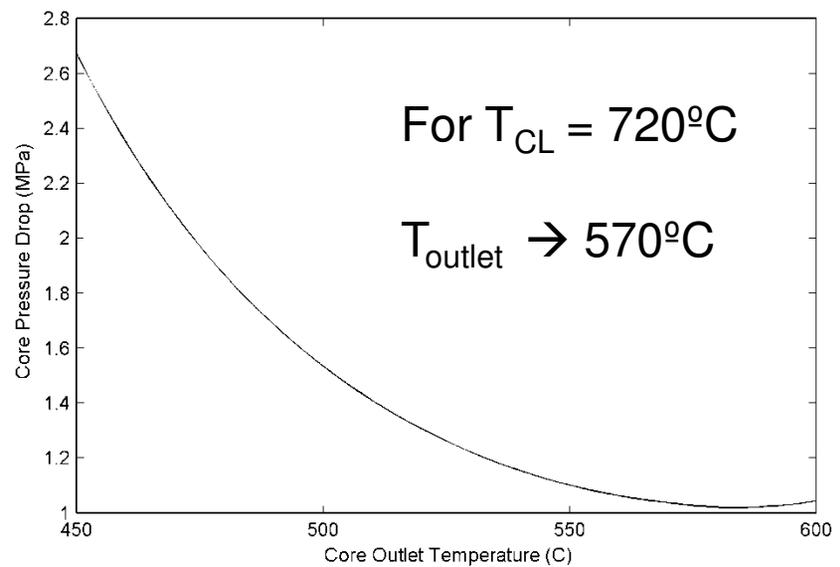
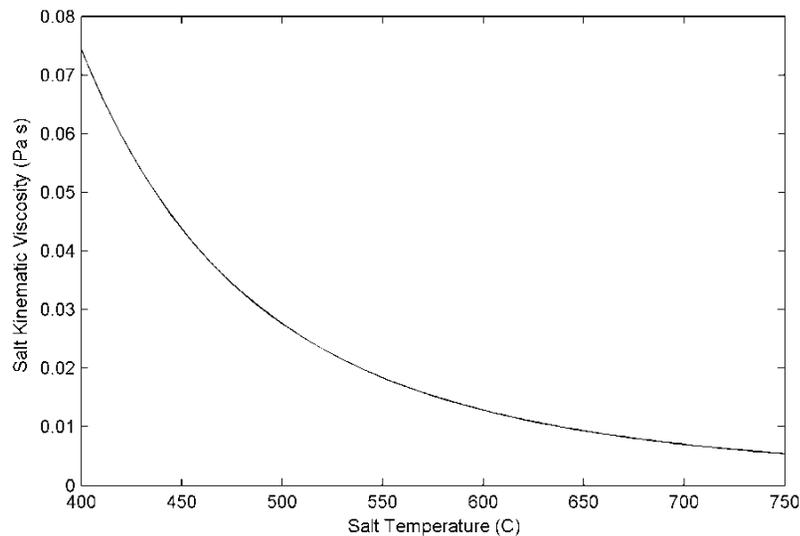
# Core Thermal Hydraulics

- Core geometry,  $T_{CL}$ , and  $q'(z)$  fixed
- Varied outlet temperature ( $T_o$ ) and to minimize  $\Delta P$

Competing effects:

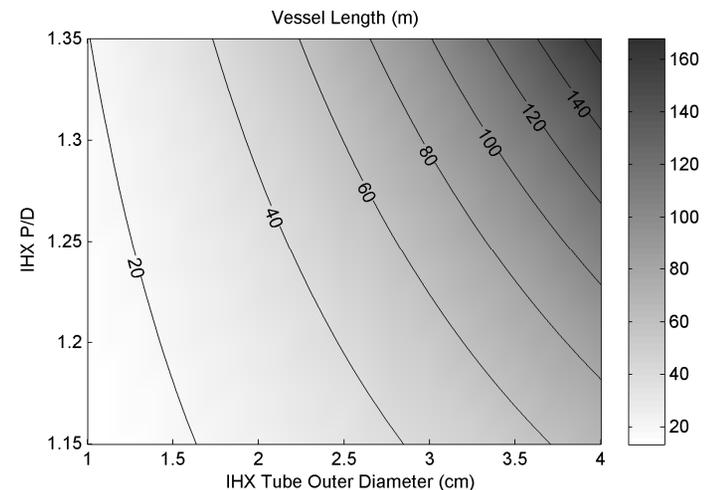
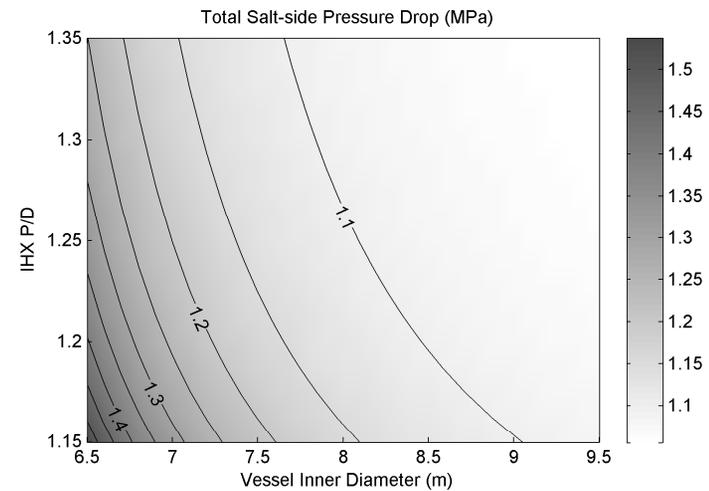
- For a fixed  $q'(z)$  and  $T_{CL}$ , a higher  $T_o \rightarrow \Delta P$  increases
- But salt viscosity decreases with  $T_o \rightarrow \Delta P$  decreases

$$q'(z) = \frac{T_{CL} - T_{bulk}}{R}$$



# IHX and Vessel Diam. Optimization

- For this optimization, the core inlet and outlet temperature and salt mass flow rate were held constant at the values determined by the core optimization
- Vessel Diameter was varied, as was the IHX tube outer diameter and pitch to diameter ratio (P/D)
- Tube thickness in the IHX was adjusted to maintain safe material stress limits
- Heat exchanger length was determined using  $\epsilon$ -NTU method
- This length was used to determine many important parameters such as:
  - Total pressure drop
  - Pump diameter
  - Vessel Length
  - Power Cycle Efficiency
  - $\text{SCO}_2$  pressure drop through IHX
- Using these techniques, a design was selected, described on next slide



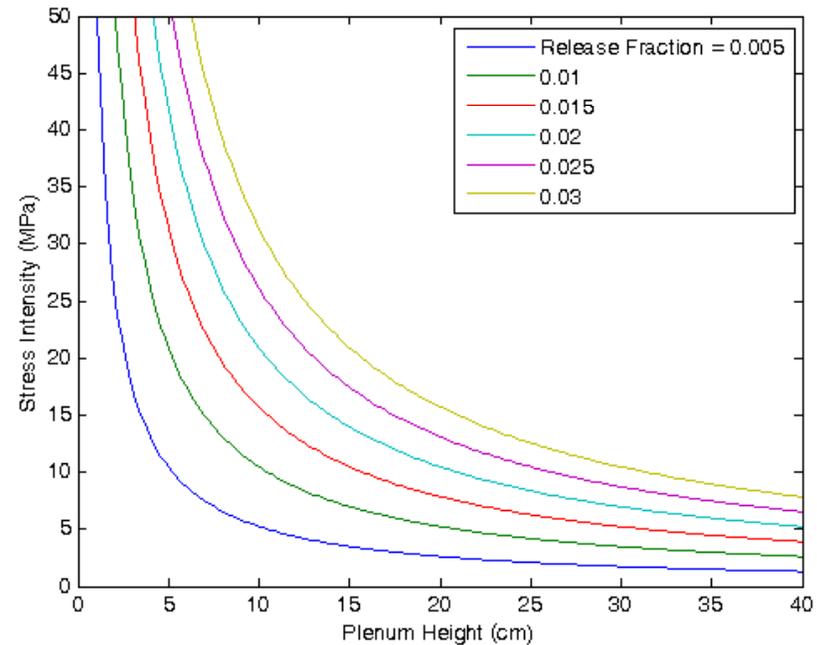
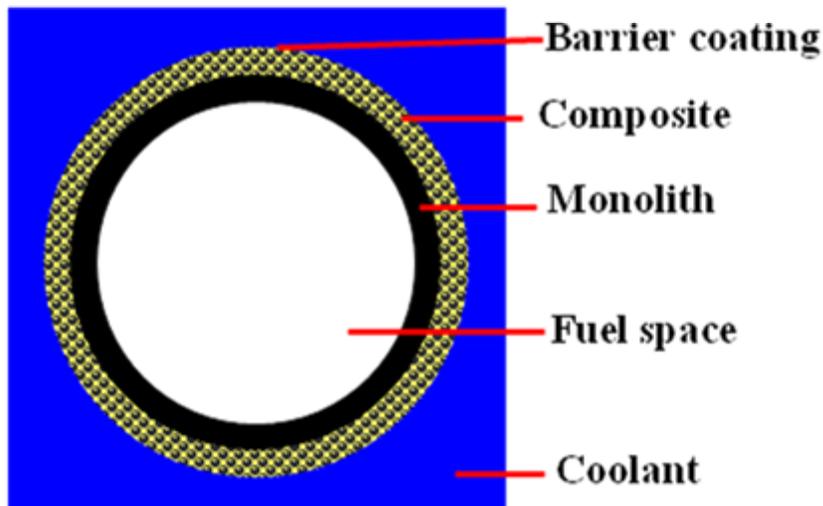
# Optimized System Properties

## System Optimization Results

Parameter	Value
Optimized Parameters:	
Vessel inner diameter	8.5 m
IHX P/D	1.2
IHX tube outer diameter	1 cm
Code Outputs:	
Vessel length	15.31 m
Margin to IHX voiding	4.1 m
Net Power Output	456.5 MW
SCO <sub>2</sub> pressure drop in IHX	19.6 kPa
Total salt-side pressure drop	1.10 MPa
Reactor vessel thickness	5.5 cm
Pump diameter (for 2 pumps)	0.63 m
IHX tube length	6.89 m
IHX tube thickness	1.7 mm
Net Cycle Efficiency	45.65%
Salt heat transfer coefficient in IHX	645.3 W/m <sup>2</sup> K
Salt velocity in IHX	0.26 m/s
Salt Reynolds number in IHX	140
SCO <sub>2</sub> heat transfer coefficient in IHX	2881 W/m <sup>2</sup> K
SCO <sub>2</sub> velocity in IHX	4.92 m/s
SCO <sub>2</sub> Reynolds number in IHX	1.31E5

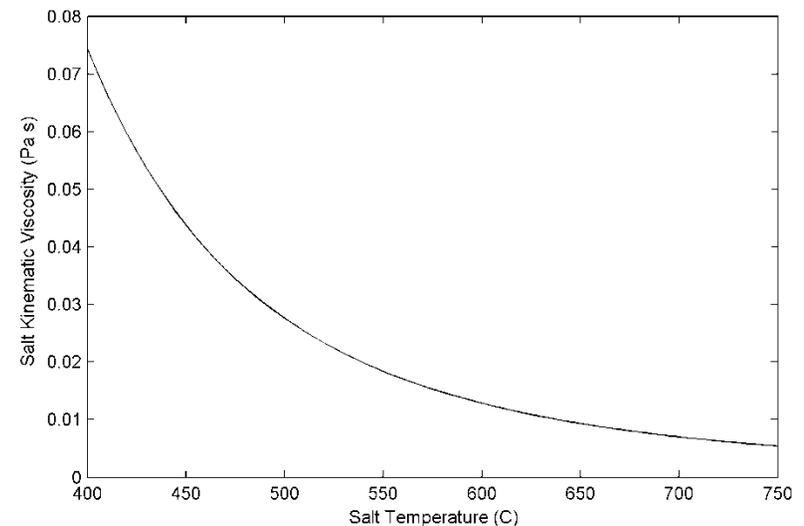
# SiC Cladding Performance

- Pb-Sn-Bi gap wide enough to prevent FCMI at desired burnups [Olander-UC Berkeley]
- FG release main cause of internal stress, unknown for high burnups
- With careful manufacturing tensile strength should be 2-300 MPa minimum; enough to withstand stress intensities of 15-20 MPa



# Minimizing Core Pressure Drop

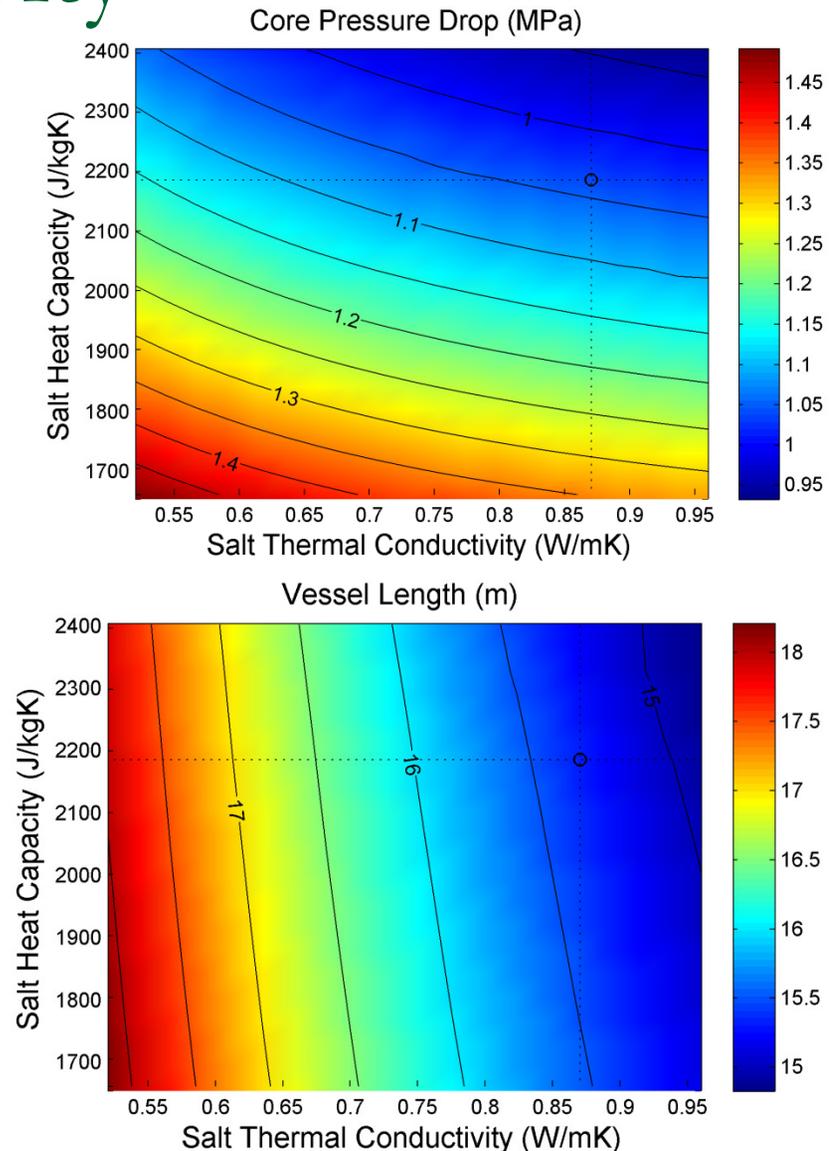
- Given assembly dimensions and linear heat rate, core flow rate is set
- To select the flow rate, core *outlet* temperature and fuel temperature limit were varied.
- Coolant velocity was increased until the peak fuel temperature was below the limit during normal operation.
- Coolant inlet temperature was simultaneously varied to maintain desired core outlet temperature.
- Results for core pressure drop is shown at top right. Given a fuel temperature limit, there is a core outlet temperature that minimizes pressure drop. The plot for 720° C fuel temperature limit is shown at bottom-right.
- Pressure drop is minimized due to temperature dependence of salt viscosity. Higher outlet temperature means higher flow rates but also reduced viscosity. These factors compete.
- For the HEER LSR, 720° C was selected as the maximum fuel temperature, and 570° C as the core outlet temperature.



$$q'(z) = \frac{T_{CL} - T_{bulk}}{R}$$

# Salt Property Sensitivity

- Since salt properties have not been extensively studied, sensitivity tests were performed.
- Thermal Conductivity was assumed in the previous design to be 0.51 W/mK. Now it is varied between 0.52 and 0.96 W/mK
- Heat Capacity was assumed to be 2186 J/kgK. For the sensitivity study it is varied between 1650 and 2400 J/kgK
- The plots on the right show the effect on core pressure drop and vessel length.
- Vessel length is still within the goals of the design. Worst case is about 18.2m
- Core Pressure Drop suffers more drastically. Worst case is just under 1.5 MPa, 50% greater than the design goal.
- This points to the need for further study of the salt in order to determine the actual values of these properties.



# Correlations Used

NaF-BeF <sub>2</sub>	
property	correlation
k	Kokhlov
Nu	4.36 for Re < 2300 Gnielinsky for Re > 2300
Nu interpolation	VDI-Warmeatlas
f	Cheng and Todreas
SCO <sub>2</sub>	
property	correlation
Nu	Gnielinsky for smooth wall Bergles et al. for ribbed design
f	Todreas and Kazimi